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ONLINE ISSN : 1349-273X

PRINT ISSN : 1346-8804

**Journal of the Japan Petroleum Institute**

Vol. 46 (2003) , No. 1 pp.53-61

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## Oxidation of Isobutane to Methacrolein over $\text{Ga}_2\text{O}_3/\text{Bi}_2\text{Mo}_3\text{O}_{12}$ Catalysts

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(Received: July 22, 2002)

Catalytic performance and the surface character of the  $\text{Ga}_2\text{O}_3$  supported Bi-Mo complex oxides were studied to achieve direct formation of methacrolein from isobutane.

$\text{Bi}_2\text{Mo}_3\text{O}_{12}$  ( $\alpha$  phase) and  $\text{Bi}_2\text{Mo}_1\text{O}_6$  ( $\gamma$  phase) showed higher catalytic activity than  $\text{Bi}_2\text{Mo}_2\text{O}_9$  ( $\beta$  phase) for isobutane partial oxidation. Supporting  $\text{Ga}_2\text{O}_3$ , which is an active catalyst for dehydrogenation of hydrocarbons, onto the oxides, enhanced the catalytic activity.

The optimum amount of supported  $\text{Ga}_2\text{O}_3$  on  $\text{Bi}_2\text{Mo}_3\text{O}_{12}$  was about 3 wt% for methacrolein formation. In the presence of oxygen, a remarkable amounts of hydrogen over  $\text{Ga}_2\text{O}_3$  during the isobutane oxidation but no hydrogen was formed over  $\text{Ga}_2\text{O}_3/\text{Bi}_2\text{Mo}_3\text{O}_{12}$ . It is confirmed from TPR that  $\text{Ga}_2\text{O}_3$  and  $\text{Bi}_2\text{Mo}_3\text{O}_{12}$  were not reduced until 550°C but the reduction of  $\text{Ga}_2\text{O}_3/\text{Bi}_2\text{Mo}_3\text{O}_{12}$  started at 350-380°C. The on-set temperature in TPR of the Bi-Mo complex oxides decreased to 350-380°C from 500°C by the supporting  $\text{Ga}_2\text{O}_3$  onto the oxides, and the catalysts after TPR measurement are composed of BiO, Bi, and  $\text{MoO}_2$  in addition to  $\text{Bi}_2\text{Mo}_3\text{O}_{12}$ . These results suggest that the hydrogen spillover took place over supported catalyst.

$\text{Ga}_2\text{O}_3/\text{Bi}_2\text{Mo}_3\text{O}_{12}$  catalyst showed higher activity and high selectivity for methacrolein at 450°C. The improvement in the selectivity for methacrolein of the  $\text{Ga}_2\text{O}_3/\text{Bi}_2\text{Mo}_3\text{O}_{12}$  may

be explained as following. Isobutane is adsorbed on the surface of  $\text{Ga}_2\text{O}_3$  to form hydrogen atom and *t*-butyl fragment and both formed species migrates to  $\text{Bi}_2\text{Mo}_3\text{O}_{12}$  surface. Migrated hydrogen may modify the  $\text{Bi}_2\text{Mo}_3\text{O}_{12}$  surface property by the reaction with oxide ions, which is active for the deep oxidation resulting in high selectivity for methacrolein.

In the non-aerobic oxidation of isobutane over the  $\text{Ga}_2\text{O}_3/\text{Bi}_2\text{Mo}_3\text{O}_{12}$  catalyst, the formation rate of  $\text{CO}_x$  significantly reduced, and methacrolein and isobutene were selectively obtained when the reduction degree of the catalyst was lower than 0.3% at 450° C.

**Keywords:** [Isobutane oxidation](#), [Methacrolein synthesis](#), [Bismuth molybdate catalyst](#), [Gallium oxide](#), [Hydrogen spillover](#), [Nonaerobic oxidation](#)

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To cite this article:

Yoshiaki OBANA, Kouji YASHIKI, Masami ITO, Hiroyasu NISHIGUCHI, Tatsumi ISHIHARA and Yusaku TAKITA, *Journal of the Japan Petroleum Institute*, Vol. **46**, No. 1, p.53 (2003) .

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doi:10.1627/jpi.46.53

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